

1

φ PVC

$$\varnothing = 70 \text{ mm} \Rightarrow r = 35 \text{ mm}$$

$$L = 200 \text{ m}$$

$$Q = 18000 \text{ L h}^{-1}$$

$$C = 150$$

F. Hazen-Williams;

$$v = 0,849 C R^{0,63} j^{0,54}$$

φ.c. m

1) a) v = ?

$$Q = A \cdot v \Rightarrow v = \frac{Q}{A}$$

$$A = \pi \left(\frac{70 \times 10^{-3}}{2} \right)^2 = 3,85 \times 10^{-3} \text{ m}^2 = 0,00385 \text{ m}^2$$

$$\Rightarrow v = 18000 \frac{\text{dm}^3}{\text{h}} \times \frac{10^{-3} \text{ m}^3}{1 \text{ dm}^3} \text{ h}^{-1} / 3,85 \times 10^{-3} \text{ m}^2$$

$$v = \frac{18000 \times 10^{-3} \text{ m}^3}{3,85 \times 10^{-3} \text{ m}^2} \cdot \text{h}^{-1}$$

$$v = \frac{18 \times 10^3 \text{ m}}{3,85} \cdot \frac{1}{\text{h}} \cdot \frac{1 \text{ h}}{3600 \text{ s}} = 1,298 \approx 1,3 \text{ m s}^{-1}$$

b) φ.c. mit.

$$v = 0,849 C R^{0,63} j^{0,54} \quad \text{φ.c. mit.}$$

$$1,3 = 0,849 \cdot 150 \times 0,0175^{0,63} \cdot j^{0,54}$$

$$R.(\text{raio hid.}) = \frac{r}{2} = \frac{0,035}{2} = 0,0175 \text{ m}$$

$$\Leftrightarrow j^{0,54} = 0,1306 \quad \Leftrightarrow (j^{0,54})^{1/0,54} = 0,1306^{1/0,54}$$

$$\Leftrightarrow j = 0,023 \text{ m} \cdot \text{m}^{-1}$$

c) L = 200 m

$$J = j \times L = 0,023 \times 200 = 4,6 \text{ m}$$

② Poucas singularidades \Rightarrow 2º método: Simplificado

$$\Sigma h_s = 0.15 \times 4.6 = 0.69 \text{ m}$$

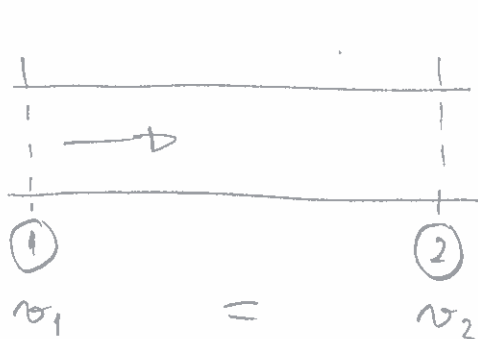
Perda de carga total (H):

$$H = \gamma + \Sigma h_s = 4.6 + 0.69 = 5.29 \text{ m}$$

↓
 assumir que as p.c. sing.
 tomam um valor em
 % de f (perdas de c.
 contínuas)

$f \cdot ex.: 15\%$

③ a) $\frac{p_1}{\gamma} = 36 \text{ m}$; tubo horizontal



$$\frac{p_2}{\gamma} = ?$$

$v_1 = v_2$ pq. ϕ é =
 (lei de continuidade $A_1 v_1 = A_2 v_2$
 logo $A_1 = A_2$; $\phi_1 = \phi_2$)

$\Delta N = 0$ (pq. o tubo é
 horizontal)
 $z_1 = z_2$

↓
 O desnível é zero

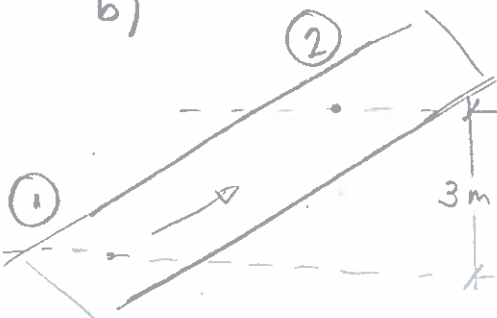
Aplicando a Eq. Bernoulli:

$$H_1 = H_2 + \Delta H_{1-2}$$

$$\frac{p_1}{\gamma} + \frac{v_1^2}{2g} + z_1 = \frac{p_2}{\gamma} + \frac{v_2^2}{2g} + z_2 + \Delta H_{1-2}$$

$$36 = \frac{p_2}{\gamma} + 5.29 \text{ m} \Rightarrow \frac{p_2}{\gamma} = 30.7 \text{ m}$$

b)



$\frac{p_1}{\gamma} = 36 \text{ m}$, tubo inclinado $\Delta N = 3 \text{ m}$
 $\frac{p_2}{\gamma} = ?$

Eq. Bernoulli:

$$H_1 = H_2 + \Delta H_{1-2}$$

$$\frac{p_1}{\gamma} + \frac{v_1^2}{2g} + z_1 = \frac{p_2}{\gamma} + \frac{v_2^2}{2g} + z_2 + \Delta H_{1-2}$$

$$36 + 0 = \frac{p_2}{\gamma} + 3 + 5.29$$

$$\Rightarrow \frac{p_2}{\gamma} = 27.7 \text{ m}$$

EXERC. II

$$L = 200 \text{ m}$$

$N = 100$ saídas

$$\Delta H = ?$$

$$y = 4,6 \text{ m}$$

$$\Delta H = y' + \sum h_s$$

$$y' = y \times F$$

PVC

Utilizámos a f. H-u

↓ calcular f

↓

$$\beta = 1,85$$

$$n = 100$$

↓

$$F = 0,356$$

$$y' = 4,6 \times 0,356 = 1,64 \text{ m}$$

$$\sum h_s = \% y'$$

$$\sum h_s = 0,20 \times 1,64 = 0,32 \text{ m}$$

↓

> * pp. cd. saída introduz uma perda de carga singular

(20% - redes médias)

* do qd c/ Q contínuo

$$\Delta H = 1,64 + 0,32 = \underline{\underline{1,96 \text{ m}}}$$

III

$$H_1 = H_2 + \Delta H + H_{mf}$$

$$L = 50 \text{ m}$$

PVC

$$\phi = 50 \text{ mm}$$

$$\frac{p}{\gamma} \text{ aspirador} = 20 \text{ m}$$

$$h_{\text{cana}} = 2 \text{ m}$$

$$\eta = 70\%$$

$$H_{mf} = ?$$

$$P_e = ?$$

$$P_b = ?$$

$$H_1 \begin{cases} v_1 = 0 & (\text{res. sds. diams.}) \\ \frac{p_1}{\gamma} = 0 & (\text{p. atm.}) \\ z_1 = 0 & (\text{referencia}) \end{cases}$$

$$H_2 \begin{cases} v_2 = \text{desprez.} \\ \frac{p_2}{\gamma} = 20 \text{ m} & (\text{alt. fig. aspirador}) \\ z_2 = 4 + 2 = 6 \text{ m} \end{cases}$$

Cálculo das perdas de carga entre ① e ②:
(ΔH)

F. H-W (aspiração)

$$v = 0,849 \text{ CR}^{0,63} j^{0,54}$$

$$v = Q/A = 0,0017 / 0,001963 = 0,849 \text{ m s}^{-1}$$

$$Q = 6 \text{ m}^3 \text{ h}^{-1} \times \frac{1 \text{ h}}{3600} = 0,0017 \text{ m}^3 \text{ s}^{-1}$$

$$A = \pi \left(\frac{50 \times 10^{-3}}{2} \right)^2 = 0,001963 \text{ m}^2$$

$$C = 150 \text{ (PVC)}$$

$$R = \frac{C}{2} = \frac{150}{2} = 75$$

$$0,849 = 0,849 \cdot 150 \cdot 0,0125^{0,63} \cdot j^{0,54}$$

$$\Leftrightarrow j = 0,0155 \text{ m m}^{-1}$$

$$j = j \times L = 0,0155 \times 50 = 0,776 \text{ m}$$

$$\Sigma h_s = 0,15 \times 0,776 = 0,1164 \text{ m}$$

$$\Leftrightarrow \Delta H = j + \Sigma h_s = 0,776 + 0,1164 = 0,89 \text{ m}$$

Eq. Bernoulli:

alt. manométrica total (H_{mf}):

$$0 + 0 + 0 = 0 + 20 + 6 + 0,89 - H_{mf} \Leftrightarrow H_{mf} = 27 \text{ m}$$

$$P_e = Q \cdot \gamma \cdot H_{mf} = 0.0017 \times 9800 \times 27 = \underline{\underline{450 \text{ W}}} \quad -2-$$

$$\gamma = \rho \cdot g = 1000 \times 9.8 \text{ N m}^{-3}$$

$$P_b = \frac{P_e}{\eta} = \frac{450}{0.7} = \underline{\underline{645 \text{ W}}}$$